OPTIMIZATION OF DRYING PROCESS PARAMETERS OF CASSAVA CHIPS IN ROTARY DRYER

ABSTRACT

Drying process parameters of cassava chips using rotary dryer was optimized using response surface method. The drying temperature, cassava chip size, drum speed and load quantity were considered as the independent variables while the moisture content, swelling index and thermal degradation of cassava chips were used as the dependent valuables. The higher and lower factor values of the four independent valuables were obtained using Minitab 17. An experimental plan was developed from the statistical tool employed which designed the experiment into 30runs. At optimal value conditions of 216^oC drying temperature, 2.5mm cassava chips size, 8.4rpm drum speed and load quantity of 6tons, the experimental results yielded 9.34% moisture content, 1.69 swelling index and 1.01% thermal degradation. The model obtained from the response surface curves were used to develop a selection chart which will be useful to control time, quality and cost of drying in Nigerian agro storage industries.

Keywords: optimization, drying, cassava chips, parameters, rotary dryer, process

1 INTRODUCTION

Preservation is one of the many steps that comes under post-harvesting of agricultural products which reduce post-harvest losses and increases food availability from existing production. In developing nations like Nigeria and other countries in Asia, Africa, and South America, 40% of total agricultural products get spoilt due to lack of proper post-harvest management method [Postharvest Management, 2006, Nachiketh et al, 2016]. Drying is an energy intensive process that results in the removal of moisture from a body by evaporation. It is also a mass transfer process consisting of the removal of water or another solvent by evaporation from solid, semisolid or liquid [Free online dictionary 2011]. This process is often used as a final production step before selling or packaging products. For a product to be considered dried the final product must be solid in the form of continuous sheet, long pieces, particles or powder. Examples are paper, wood, corn flakes, sand etc. Agricultural materials especially starchy foods such as cassava meals are hygroscopic so they can lose or absorb moisture depending on the ambient air condition [Serpil and Servet 2006]. Cassava has been established to be an important food crop in the tropics and a major source of carbohydrate with 88% of it been produced and consumed in Africa by human beings [Taiwo 2006] and statistics has shown that Nigeria is currently the largest producer of cassava in the world [FAO. 2004, 2006]. Besides serving as the primary staple food for millions of people, it can be converted into dried stable products such as chips and pellets which are useful as basic raw material in animal feed formulations, ethanol

production and cassava beer [Ashaye, 2005]. Processing the tubers into chips reduces the moisture content to a very low level and reduce post-harvest losses. According to Kuye et al (2004), These cassava chips are marketed locally in all the southern states in Nigeria to a tune of 1500tons per day. [Rasaq, 2019] it was reported that 10 - 40% of yam lost to post-harvest are due to lack of appropriate storage facilities. Ademiluyi (2016) developed a software for design and construction of rotary dryer for drying ground cassava. Its drying stage determines the quality of the dried chips produced bearing in mind that undesirable biochemical changes, subsequent contamination and spoilage of the chips can only be prevented if the drying process is fast enough and the final product is dry enough [Maskan 2000]. Cassava has high moisture content which if not removed within 72 - 92 hours will cause the growth of microorganism in the cassava which eventually will spoil the cassava. Cutting these cassava roots into chips are the most common form in which dried cassava root are marketed and still retain its rich nutrients. Rasaq (2019) did an analysis on a biogas driven combined cooling, heating and power generation system that harmonizes power generation with food drying and cold storage to solve the problem of heavy post-harvest loss in the sub-Saharan African region because they lack clean energy. They proposed a system that is able to dry 816.73 T of cassava tubers, 267.33 T of maize and cold-store 3.365 T of tomato every year. Rasaq (2019) did a review on the contributions of combined power and drying, application of phase change materials and hybrid drying systems with regard to agricultural products. They indicated that deployment of biomass powered combined heat and power systems might be a good solution to post-harvest wastes since both electricity and heat for drying of agricultural products can be simultaneously obtained. However, as these challenges have established that drying will help save post-harvest lost, no work has been done on its process parameter been the main objective of this work which is to optimize the drying process parameters of cassava chips in rotary dryer with the specific objectives of developing a mathematical model for the process, developing a selection chart for cassava chips drying process parameter using a rotary dryer for industrial use and optimizing the drying temperature, cassava chip size, drum speed and load quantity using response surface method approach.

2. MATERIALS AND METHOD

The cassava used for this work was sourced from Nweke J. C. farm in Nenwe, Aninri L.G.A., Enugu state. The back was peeled with a knife and cut into chips of various dimensions using cassava chipping machine and weighted.

Moisture Content was calculated using equation 1

$$Mc(\%) = \frac{Wi - Wf}{Wi} \times 100 \tag{1}$$

Where $W_{i=}$ initial weight of cassava chips and W_{f} = final weight of cassava chips

The Swelling Index: After drying the cassava chips, it was introduced into a 1000ml measuring cylinder, the initial volume (V_i) was recorded and water was added to fill the cylinder to the brim, the set up was allowed to settle for 20minutes then the final volume (V_f) was taken to calculate the swelling index, using equation 2. $Si = \frac{V_f}{V_i}$ (2)

Thermal Degradation: The dried cassava chips were weighed; the burnt cassava chips were selected and also weighed. The thermal degradation was calculated using equation 3.

$$Td(\%) = \frac{W_b}{W_{tot}} \times 100 \tag{3}$$

Where W_b = weight of burnt cassava chips and W_{tot} = total weight of dried cassava chips

Drying Efficiency: the drying efficiency was calculated using equation 4 according to Matuam et al (2015) $\eta = \frac{m_c * L_c}{A_c * C_c * \Delta T}$ (4)

Where m_c is mass of water evaporated from the cassava chips(kg), L_c is latent heat of vaporization (kj/kg), A_c is mass of air (kg), C_c = specific heat of air (kj/kg⁰C), ΔT = temperature difference (⁰C)

Equilibrium Moisture Content: the equilibrium moisture content of cassava chips were calculated using equation 5 according to Mitchell (2018).

$$E_{mc} = \frac{1800}{V} \left[\frac{(kN_C)}{1 - kN_C} + \left(\frac{K_{C_1} KN_C + 2K_{C_1} K_{C_2} K^2 N_C^2}{1 + K_{C_1} KN_C + K_{C_1} K_{C_2} K^2 N_C^2} \right) \right]$$
(5)

Where E_{mc} the equilibrium moisture is content, N_c is relative humidity and V, K, K_{c1} , K_{c2} are coefficients which were calculated using equations 6 -9.

$$V = 330 + 0.452T + 0.00415T^{2}$$
(6)
$$V = 0.701 + 0.000462T = 0.000000844T^{2}$$
(7)

$$\mathbf{K} = 0.791 + 0.000463\mathrm{T} - 0.000000844\mathrm{T}^2 \tag{7}$$

$$K_{C1} = 6.34 + 0.000775T - 0.0000935T^2$$
(8)

$$K_{C2} = 1.09 + 0.0284T - 0.0000904T^2$$
(9)

Where T is the dry bulb temperature.



Figure 1: Rotary Dryer

The rotary dryer is made of stainless steel with a capacity of 9.3 tonnes per hour and dimensions of 880mm diameter, 1770mm height and 3660mm length. It has a heat source, an electric motor, air blower and the drying chamber. The optimization of the settings and the empirical relationships between the drying process parameters (factors) and responses in rotary drying of cassava chips were analyzed by response surface method approach. This involves Response Surface Method (RSM) experimental design, evaluation and modeling such as model fitting, selection and development of established optimal parameter table for cassava chips drying.



3mm thickness4mm thicknessFigure 2. Cassava Chips granulometric classification pictures

2.1: Procedures for optimization of cassava chips drying process.

Evaluation, modeling and optimization of cassava chips drying process involves:

- a. Development of appropriate RSM experimental plan.
- b. Selection of a response surface model.
- c. Optimization of the selected models.
- d. Verification/confirmation of the modeling and optimization results.

Design of experiment choice was based on variables number, objective of study, resource availability and source of data collection. Cassava drying in rotary dryer process parameters – drying temperature, cassava chips size, Drum speed, Load quantity on moisture content, swelling index and thermal degradation were studied. [Minitab software, Version 17. 2006] was used to generate 30 experimental runs to study variable number (K = 4) for independent variables including drying temperature (D_t), cassava chips size(C_s), Drum speed(D_s), Load quantity(L_q), were used for the design. These independent variables constitute the factors and were coded as x_1 , x_2 , x_3 and x_4 respectively. The responses of Moisture content (M_c), swelling index(S_i) and thermal degradation (T_d) were calculated using the results of the experimental runs. The search for models that will describe the responses adequately started with fitting of linear function due to desire to quantify the parameters with simplest possible functions. The limits for cassava chips drying process parameters. The axial point value was augmented to ±2.336 since the typical α of (+2,-2) could not give significant models. The 0 level, -2.336 and +2.336 were calculated by interval addition in Minitab, and a design matrix was obtained.

		Factor	r Symbols	Facto	r Values
S/N	Factor Description	Coded	Actual	High (+1)	Low (-1)
1	Drying temperature (⁰ C)	<i>x</i> ₁	D _t	200	160
2	Cassava Chips Size (mm)	<i>x</i> ₂	Cs	5	3
3	Drum Speed(rpm)	<i>x</i> ₃	D _s	14	10
4	Load quantity (tons)	<i>x</i> ₄	L _q	9	6

Table 1: Limits of cassava chips drying process Parameters

The choice of centre points offers a logical balance among the strength, durability and economic considerations associated with the objective of this study. The Moisture content (M_c) , swelling index (S_i) and thermal degradation (T_d) are the actual values of cassava chips drying process responses in their original/ natural units. Thereafter, the natural values of these responses were determined using the transformation equations 1 which relate the coded and actual values of the

factors [Agunwamba 2007]
$$X = \frac{x - \left(\frac{x \max + x \min}{2}\right)}{\left(\frac{x \max - x \min}{2}\right)}$$
(10)

Coded variable is denoted as X and natural units of independent variable is x, then maximum and minimum independent factors respectively are x_{max} and x_{min} .

Experii Runs	nental		Coded	l Values		Actual Values			
Std Order	Run Order	X1	X2	X3	X4	Drying Temperature (⁰ C)	Cassava Chip Size (mm)	Drum Speed (rpm)	Load Quantity (tons)
1	1	-1	-1	-1	-1	160	3	10	6
2	2	1	-1	-1	-1	200	3	10	6
3	3	-1	1	-1	-1	160	5	10	6
4	4	1	1	-1	-1	200	5	10	6
5	5	-1	-1	1	-1	160	3	14	6
6	6	1	-1	1	-1	200	3	14	6
7	7	-1	1	1	-1	160	5	14	6
8	8	1	1	1	-1	200	5	14	6
9	9	-1	-1	-1	1	160	3	10	9
10	10	1	-1	-1	1	200	3	10	9
11	11	-1	1	-1	1	160	5	10	9
12	12	1	1	-1	1	200	5	10	9

Table 2: RSM design table for cassava chips drying process parameters

13	13	-1	-1	1	1	160	3	14	9
14	14	1	-1	1	1	200	3	14	9
15	15	-1	1	1	1	160	5	14	9
16	16	1	1	1	1	200	5	14	9
17	17	0	0	0	0	180	4	12	7.5
18	18	0	0	0	0	180	4	12	7.5
19	19	0	0	0	0	180	4	12	7.5
20	20	0	0	0	0	180	4	12	7.5
21	21	-2.336	0	0	0	132.68	4	12	7.5
22	22	2.336	0	0	0	227.32	4	12	7.5
23	23	0	-	0	0	180	1.634	12	7.5
			2.336						
24	24	0	2.336	0	0	180	6.366	12	7.5
25	25	0	0	-	0	180	4	7.268	7.5
				2.336					
26	26	0	0	2.336	0	180	4	16.732	7.5
27	27	0	0	0	-	180	4	12	3.951
					2.336				
28	28	0	0	0	2.336	180	4	12	11.049
29	29	0	0	0	0	180	4	12	7.5
30	30	0	0	0	0	180	4	12	7.5

The search for models that will describe the responses adequately started with fitting of linear function because of the desire to quantify the parameters with simplest possible functions. However, failure of the test for adequacy requires the ascension to the next order level until a satisfactory and adequate model is developed. The 0 Level i.e control value for all the variables (cassava chips drying process parameters) that will be used for the experiment are determined from the machine operation specifications. The limits of cassava chips drying process parameters are shown in table 1. in each of the tests for the determination of the actual levels for any of the factors, the other three factors were kept constant at their design values. According to Eze et al (2017), Thermal degradation which is characterized by darkening colour change was also used for determining the high level operational parameter limit for drying temperature. In line with Murray and Lary (2008) study the cassava chips rotary dryer process parameter design generated was subsequently approximated with a regression equation and used to develop models for predicted response, Y i.e. Moisture content (M_c), swelling index(S_i) and thermal degradation (T_d) of constant (intercept), β_0 with linear coefficient, β_i , and cross product coefficient. x_i and x_j are the coded independent variables, β_{ij} , in the form

$$Y = \beta_0 + \sum_{j=1}^k \beta_j \, x_j + \sum_{j<} \sum_{j=2}^k \beta_{ij} x_i x_j \tag{11}$$

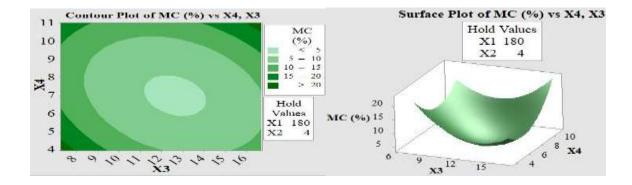
Equation 11 is used to predict response surface models with quadratic effects and two factor interaction for Moisture content, swelling index and thermal degradation as affected by the cassava chips rotary dryer process parameters namely Drying Temperature, cassava chip size, Drum speed and Load quantity [Nicolai et al 2004]. The response design comprises of two level factorial points (-1, 1), center points (0) and axial points ($\alpha = \pm 2.336$) for each independent variable to estimate the second order polynomial while the best overall design occurs at $\alpha = \sqrt[4]{nf}$ and n = 30 for a blocked design [Murray and Lary 2008].

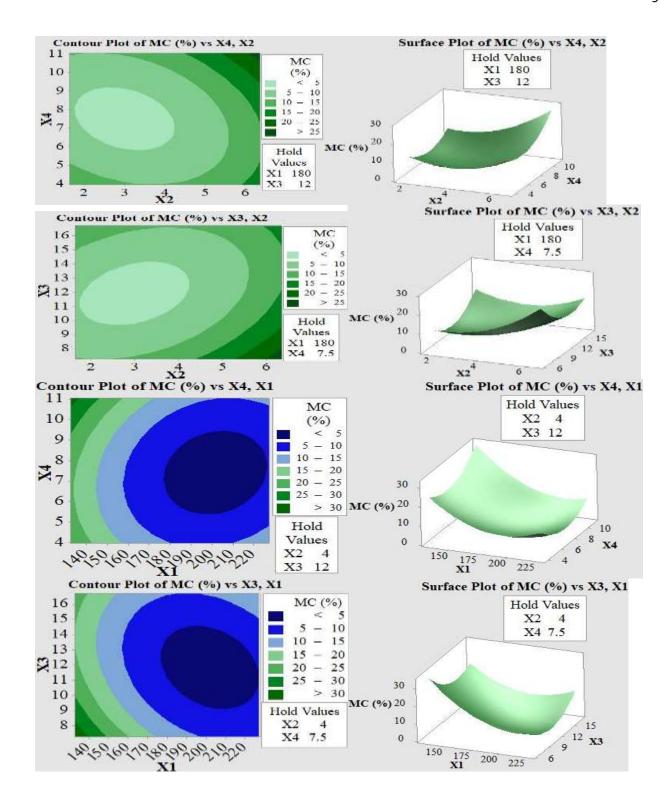
$$Y = \beta_0 + \sum_{j=1}^k \beta_j x_j + \sum \beta_{jj} x_j^2 + \sum_{j<} \sum_{j=2}^k \beta_y x_i x_j$$
(12)

Considering a need to quantify the parameters with simplest possible functions, the search for models that will describe the responses adequately started with fitting of linear function. The optimized responses and factors were subjected to desirability function analysis to get the actual desired responses as influenced by the cassava chips rotary drying process parameters. The values obtained from the desired responses were used for development of selection chart that will serve as a guide for cassava chips drying in rotary dryer.

3. RESULT AND DISCUSSIONS

Figures 3 to 5 depicts the 3D response surface curve for cassava chip quality against drying process parameters of cassava chips, the desirable factor of 11.1% and 10.8% is the one that minimizes the cassava chip moisture content (MC) for x3 and x4, these optimum response was attained at center point in the curve for x3, x4, while 20.3% x1 depicted maximum point and 15.2% minimum value of x2





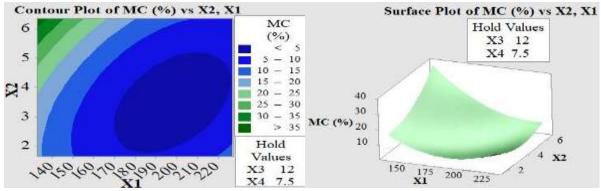
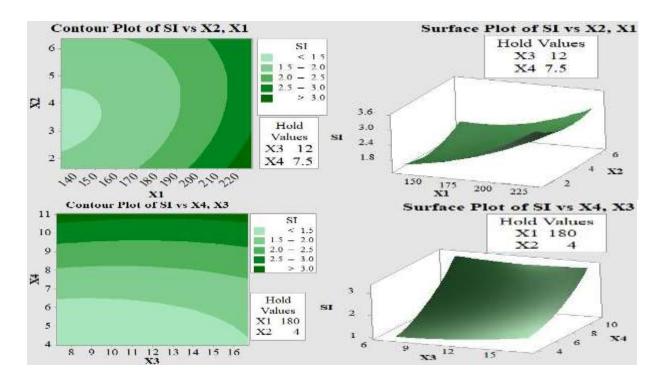


Figure 3: RSM Plot of Cassava chip MC (%) against drying process Parameters.

In Figure 4, the optimization goal here is to maximize swelling index of cassava chips, As depicted in the 3D curves, a stationary response surface ridge pattern and the desirable response was optimum at maximum values of 2.9 and 3.3 for x1 and x4 and minimum values of 2.1 and 2.0 for x2 and x3. The lighter shades indict the optimum points from the contour plots.



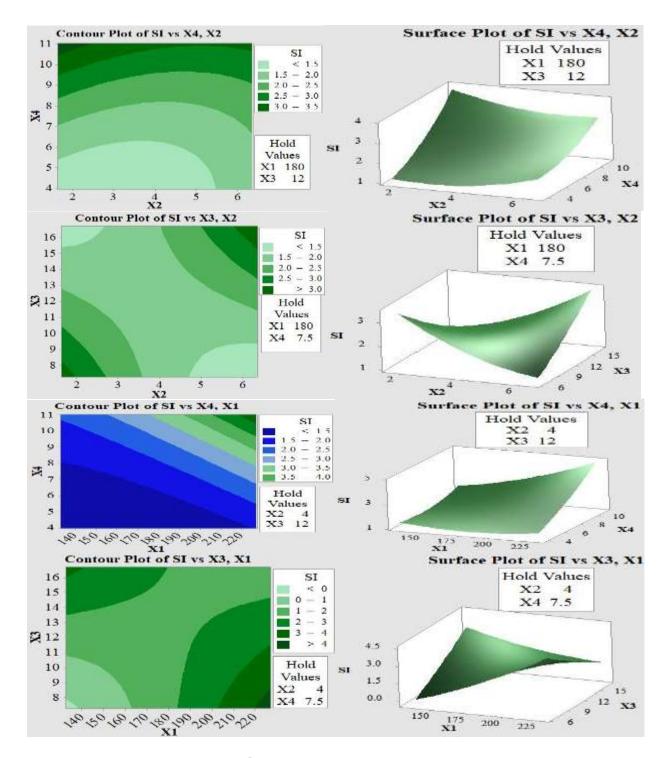
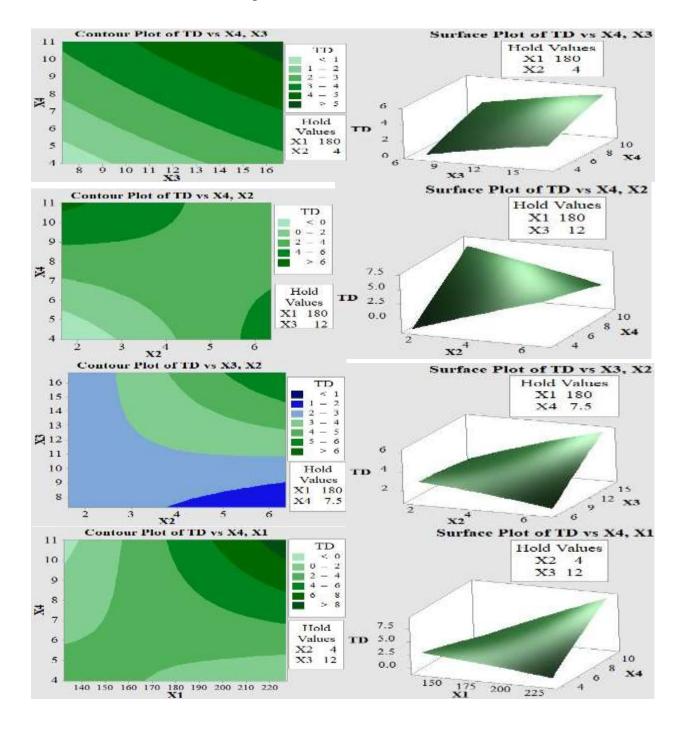


Figure 4: Contour/surface Plot of cassava chips SI against drying process Parameters. Response surface plots of thermal degradation of cassava chips are shown in Figure 5, all the response surface plots exhibited a minimal ridge response surface pattern. The desirable response of 1.2%, 2.3%, 1.8% and 1.5% were attained at drying temperature (x1), cassava chips



(x2), drum speed(x3) and load quantity(x4) respectively which minimizes thermal degradation for x1, x2, x3 and x4 at a minimal point values.

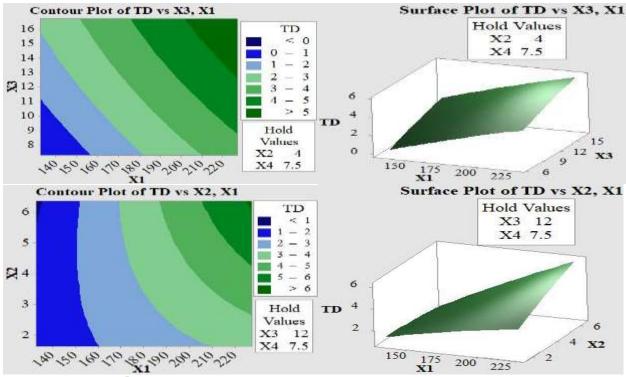


Figure 5: RSM Plot of cassava chip TD against drying process Parameters.

Kathleen et al (2004) observed that optimization using the response surface – contour and surface plots – is technically unreliable when there are more than one response and multiple predictors. Thus it can lead to multiplicity of optimal settings established for one response. Inspection of the contour and surface graphs revealed that for a particular response, some factor pairs are in the maximum region while others indicate minimum optimal region. The indeterminate tendency of this approach gave rise to the need to adopt a more suitable optimization approach which can define the optimal settings of the cassava chips drying process parameters for all the responses.

The desirability function optimization plots are shown in Figures 6 as obtained by the application response optimizer capability of Minitab software, Version 17. 2006.

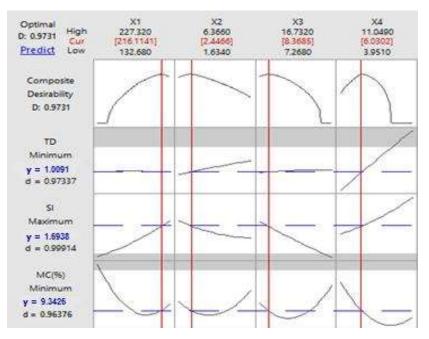


Figure 6: Improved cassava chips drying Process Optimization Plot.

Parameters	SON standard	Stephensule et	Lateef et	My work				
	2004	al 2017	al 2015					
Moisture content (%)	13% maximum	11.85	8.78	9.34				
Swelling index	-	-	1.72	1.69				
Thermal degradation	-	-	-	1.01				
(%)								

Table 3: Comparison of my cassava chips study with other works

Equations (13) to (15) are the models for calculating the cassava chips quality as influenced by the drying process parameters. These empirical relationships were obtained from the response surface plots of cassava chips quality against drying process parameters. The drying efficiency before optimization was 17.6% whereas drying efficiency after optimization was 20.3% producing a drying efficiency difference of 2.7%. The equilibrium moisture content was calculated as 12.8%

$$\begin{split} M_{C}(\%) &= 245.2 - 1.457 D_{T} + 4.71 C_{S} - 11.80 D_{S} - 9.82 L_{Q} + 0.003855 D_{T} D_{T} + 1.042 C_{S} C_{S} + \\ &0.3274 D_{S} D_{S} + 0.561 L_{Q} L_{Q} - 0.0546 D_{T} C_{S} + 0.01881 D_{T} D_{S} - 0.0142 D_{T} L_{Q} - 0.359 C_{S} D_{S} + \\ &0.421 C_{S} L_{Q} + 0.223 D_{S} L_{Q} \end{split}$$

$$\begin{split} S_I &= \\ &-3.68 + 0.0232 D_T - 1.065 C_S + 0.903 D_S - 0.638 L_Q + 0.000155 D_T D_T + 0.0630 C_S C_S + \\ &0.00439 D_S D_S + 0.02796 L_Q L_Q - 0.00175 D_T C_S - 0.007342 D_T D_S + 0.00412 D_T L_Q + \\ &0.0972 C_S D_S - 0.0395 C_S L_Q - 0.0073 D_S L_Q \end{split}$$

$$\begin{array}{c} D_{D}(70) = 12.01 & 0.1054D_{T} + 0.130C_{S} & 0.140D_{S} & 1.141L_{Q} & 0.000001D_{T}D_{T} \\ 0.0243C_{S}C_{S} - 0.00546D_{S}D_{S} - 0.0108L_{Q}L_{Q} + 0.00737D_{T}C_{S} + 0.00013D_{T}D_{S} + \\ 0.01850D_{T}L_{Q} + 0.1248C_{S}D_{S} - 0.3383C_{S}L_{Q} - 0.0010D_{S}L_{Q} \\ (15) \end{array}$$

where:

M_C = Moisture Content		$D_S = Drum Speed$	C_S = cassava chip size
$S_I = Swelling Index$		D _T = Drying Temperature	$L_Q = Load Quantity$
T_D = Thermal Degradation	1		

Cassava	Drying	Cassava chip	Drum	Load
drying quality	temperature(^o C)	size(mm)	speed(rpm)	quantity(tons)
Moisture				
Content (%)				
2.5	227.0	1.0	13	1.00
5.0	204.5	1.8	12	1.50
7.5	182.0	3.0	12	2.50
10.0	159.0	5.0	12	3.75
12.5	150.0	5.8	8	7.50
15.0	141.0	6.0	5	11.5
17.5	132.0	7.0	3	15.25
20.0	125.0	7.5	3	19.50
22.5	118.0	8.0	3	23.00
25.0	111.0	8.2	1	27.50
Swelling				
Index				
1.00	228	19	25	12
1.25	222	16	23	11
1.50	216	13	21	10
1.75	210	10	19	9.5
2.00	204	7	17	8.5
2.25	197	3.8	15	7.5
2.50	168	4.0	9	7.0
2.75	140	4.2	3	6.5
3.00	112	4.6	3 3	4.5
3.25	84	4.6	3	2.5
Thermal				
Degradation (%	(0)			
0.5	236	8.0	17	13.4
1.0	225	7.0	16	11.6
1.5	210	5.6	15	9.8
2.0	195	4.2	14	8.5
2.5	180	2.8	11	6.7

3.0	165	1.8	10	5.8	
3.5	150	0.8	7	4.5	
4.0	135	0.7	4	3.2	
4.5	120	0.3	3	1.9	
5.0	105	0.2	2	0.6	

4. CONCLUSION

From the results of the findings, the following conclusions can be drawn

- That optimal values of the drying process parameters were gotten at the optimal settings of 216^oC, 2.5mm, 8.4rpm and 6.0tons for values of drying temperature, cassava chip size, drum speed and load quantity respectively
- That equation 13, 14 and 15 should be used in simulation of the expected responsesmoisture content, swelling index and thermal degradation during the drying process of cassava chips using rotary dryer with respect to the parameters; drying temperature, cassava chip size, drum speed and load quantity.
- That an optimal value of 9.34% moisture content, 1.69 Swelling Index and 1.01% thermal degradation were gotten for cassava chip drying process using rotary dryer
- That the selection chart should be used for optimization of cassava chip drying process with respect to time, quality and cost as the need be.

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